

การเหนี่ยวนำยีสต์ *Moniliella* sp. BCC25224 ให้กลายพันธุ์ด้วยรังสียูวีและเอทิลเมทิลซัลโฟเนต (EMS) เพื่อการผลิตเอริทริทอล

Mutagenesis induction of *Moniliella* sp. BCC25224 using combination of UV and ethyl methanesulfonate (EMS) for erythritol production

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### บทคัดย่อ

เอริทริทอลคือสารให้ความหวานพลังงานต่ำที่ไม่ส่งผลต่อระดับน้ำตาลในเลือดผลิตจากการหมักกลูโคสด้วยยีสต์ *Moniliella* sp. (ยีสต์ผ่านการรับรองให้ใช้ในอาหาร) โดยงานวิจัยนี้มีวัตถุประสงค์เพื่อปรับปรุงและคัดเลือกยีสต์สายพันธุ์ *Moniliella* sp. ให้ผลิตเอริทริทอลสูง ด้วยการเหนี่ยวนำให้เกิดการกลายพันธุ์ในยีสต์ *Moniliella* sp. BCC25224 โดยใช้สารเคมีเอทิลเมทิลซัลโฟเนต (EMS) ร่วมกับฉายแสงรังสียูวีเป็นเวลา 15, 30 และ 60 นาที จากการศึกษาพบว่าสามารถคัดเลือกยีสต์ *Moniliella* sp. BCC25224-M13 ที่สามารถผลิตเอริทริทอล (erythritol production) สูงกว่าสายพันธุ์ดั้งเดิม 1.2 เท่า ( $44.2 \text{ gL}^{-1}$ ) ในระดับฟลasks โดยสามารถผลิตเอริทริทอล (erythritol production), ให้ผลได้ของเอริทริทอล (erythritol yield) และมีประสิทธิภาพการผลิตเอริทริทอล (yield coefficients) ในระดับถังหมักขนาด 10 ลิตร เท่ากับ  $103.5 \text{ g}$  ต่อลิตร,  $56.9\%$  และ  $0.59 \text{ g}$  เอริทริทอล/กรัมกลูโคส ตามลำดับ ดังนั้นการศึกษานี้จึงเป็นการพัฒนาและปรับปรุงยีสต์สายพันธุ์ *Moniliella* sp. และได้ *Moniliella* sp. BCC25224-M13 เป็นทางเลือกในการผลิตเอริทริทอล

คำสำคัญ: เอริทริทอล *Moniliella* sp. กระบวนการหมัก การชักนำการกลายพันธุ์

### Abstract

Erythritol is a safe, non-caloric and non-insulinemic sweetener present in various foods. It can be produced from glucose as substrate via fermentation with *Moniliella pollinis* (a safe and suitable food-grade osmophilic yeast). This study aims to screen high erythritol producing *Moniliella* sp. strains via mutagenesis. The candidate producer, *Moniliella* sp. BCC25224, was mutated sequentially by UV irradiation and immersion in ethyl methyl sulphonate (EMS) for 15, 30, and 60 min. The mutant named *Moniliella* sp. BCC25224-M13 was selected based on the highest levels of erythritol production at flask scale ( $44.2 \text{ gL}^{-1}$ ) which was 1.2-fold improved compared with its wild parent. In a 10-L bioreactor, the erythritol production, erythritol yield and yield coefficients by BCC25224-M13 were  $103.5 \text{ gL}^{-1}$ ,  $56.9\%$  and  $0.59 \text{ gg}^{-1}$ , respectively. This study revealed that *Moniliella* sp. BCC25224 could be used as a parent to produce mutants for superior erythritol production, such as *Moniliella* sp. BCC25224-M13.

**Keywords:** Erythritol, *Moniliella* sp., Fermentation, Mutagenesis

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## Introduction

Erythritol is a unique member of the polyol family which has sweetening organoleptic properties of 70% relative to sucrose (Rzechonek *et al.*, 2018). Erythritol can therefore be used to produce no-sugar added, reduced-sugar, or sugar-free alternatives in food, beverages and pharmaceutical products. The ingestion of erythritol has many benefits which include zero-calories, non-insulinemic, non-cariogenic, non-acidogenic, non-laxative, anti-oxidative properties and increases in malabsorption of fructose (Jacqz-Aigrain *et al.*, 2015, den Hartog *et al.*, 2010, Moon *et al.*, 2010).

Industrial production of erythritol via fermentation utilizes glucose or hydrolyzed wheat or corn starch as substrate for microbial activity. Microbial strains such as *Aureobasidium* sp. (Guo *et al.*, 2016), *Moniliella* sp. (Lin *et al.*, 2010), *Trichosporonoides* sp. and *Yarrowia lipolytica* (Xiaoyan *et al.*, 2017) have been studied for erythritol production (Rzechonek *et al.*, 2018). *Moniliella* sp. and *Yarrowia* sp. were proven to be safe for use in food processing (Rzechonek *et al.*, 2018). Nevertheless, the search for strains of *Moniliella* sp. and *Yarrowia* sp. for high erythritol yield and productivity are key for commercial production, and process conditions (Rakicka-Pustułka *et al.*, 2020). In screening and isolating of novel erythritol producing organisms, pollen, honey, beehives, preserved fruits, dry fruit and sugarcane factory's soil have served as sources (Lin *et al.*, 2001).

However, one sure way for screening and isolating superior microbes for a metabolite of interest is by genetic engineering and mutation via UV radiation or chemical mutagenesis by using ethyl methanesulfonate (EMS) (Park *et al.*, 2019, Yan *et al.*, 2021). The widely used technique is mutagenesis followed by selection because of lower cost and sophistication of processes involved. Mutation selection is an efficient and rapid way to obtain desirable traits in crop plants and microbes (Yan *et al.*, 2021) 2021.

UV mutagenesis technique has been applied to isolate yeasts for specific products such as for improved aroma production. Despite obtaining new strains by UV mutagenesis, they are designated as genetically modified organisms (GMO) by the European

Union legislation (Article 2 of EU Directive 2001/18/EC). Meanwhile, such organisms do not undergo strict regulation relative to other altering genetic modification techniques in producing GMO because of the long-standing safety record (Dederer & Hamburger, 2022). Random mutagenesis by UV emission revealed that a mutant of *Aureobasidium pullulans* CGMCC3.0837 (ER 35) produced more erythritol than parent strains by 50.92% (Guo *et al.*, 2016). In other instance, EMS was used to obtain a *Candida magnoliae* mutant with minimum by-product production (Ghezelbash *et al.*, 2014). The interaction of UV mutagenesis and chemical mutagenesis to obtain high production of erythritol is still an ongoing study.

*Moniliella* species are regarded as efficient erythritol producers. However, mutagenesis techniques are still applied to screen for superior desired traits among living organism. In this study, a sequential mutagenesis of UV radiation and EMS was applied on *Moniliella* sp. BCC25224 strain to obtain mutants capable of high erythritol production.

## Materials and methods

### Chemicals

Yeast extract was purchased from DIFCO (Detroit, MI, USA). Corn steep liquor was obtained from Friendship Corn Starch Co., Ltd. (Thailand). Soy bean flour was obtained from Win Change Industries Co., Ltd. (Thailand). Ethyl methyl sulphonate (EMS) was purchased from Sigma-Aldrich. All chemicals used were reagent grade.

### Experimental designs

The research design used was completely randomized design (CRD). The strains was treatment and each treatment was performed in triplicate. The analyst data were dry cell weight, glucose consumption, erythritol production and erythritol yield.

### *Moniliella* sp. BCC25224 cultivation and multiplication

*Moniliella* sp. BCC25224 used in this study was obtained from the BIOTEC Culture Collection (BCC), National Center for Genetic Engineering and Biotechnology, Thailand. *Moniliella* sp. BCC25224 was streaked on glucose yeast extract (GYE) agar (300 gL<sup>-1</sup>,

glucose; 10 gL<sup>-1</sup>, yeast extract, and 20 gL<sup>-1</sup> of agar) to obtain single colonies. After, cell multiplication of *Moniliella* sp. BCC25224 was carried out in a 100-mL of glucose yeast extract broth in 500-mL flasks in a shaking incubator at 200 rpm at 30°C for 5 days before use (Lin *et al.*, 2010, Burschaper *et al.*, 2002).

#### **Mutagenesis of *Moniliella* sp. BCC25224 via UV and EMS**

The mutagenesis protocol was modified from Savergave *et al.* (2011). The culture broth was centrifuged at 4,000 x g for 10 minutes and the cells were washed twice with sterile saline. Five milliliter of cell suspension (1 x 10<sup>6</sup> cell mL<sup>-1</sup>) was irradiated by Philips 30W G30 T8 lamp at wavelength 254 nm for 3 minutes at a distance of 20 cm. The cell suspension was then treated with 20 µL EMS at a final concentration of 4 µLmL<sup>-1</sup> and incubated for three different periods (15, 30 and 60 minutes). The EMS was inactivated by adding 0.5 mL of sterile sodium thiosulfate (50 gL<sup>-1</sup>). The treated cell suspension was washed twice with sterile saline before spread plating on the GYE agar medium. The plated media were incubated at 30°C for 7 days (Guo *et al.*, 2016).

Mutated colonies that survived were picked up and cultivated in GYE broth medium for 2 days at 30°C and 200 rpm for the erythritol production test. The inoculum (20 gL<sup>-1</sup>) was transferred into 100-mL GYE broth and incubated at 30°C, at 200 rpm mechanical shaker for 5 days. The fermented broth was centrifuged at 4,000 x g for 10 min at 4°C, the supernatant was then filtered through 0.45 µm nylon filter before erythritol analysis via HPLC. The strain with the highest erythritol production and highest glucose consumption were compared with the parent strain and chosen (Ghezelbash *et al.*, 2014, Lin *et al.*, 2010) for further investigation in a 10 L jar fermenter.

#### **Production of erythritol in fermenters**

*Moniliella* sp. BCC25224 and selected mutant strains were grown in a 10 L B. E. Marubishi fermenter containing 5 L broth (200 gL<sup>-1</sup> glucose and 13 gL<sup>-1</sup> soybean flour, pH 5.3) with agitation speed of 350 rpm and aeration rate of 0.7 vvm at 30°C. Broth samples were harvested and analyzed every 11 or 12 hours for 9 days to calculate the dry cell weight, erythritol concentration, glucose consumption, erythritol yield, yield coefficients and productivity.

#### **Physico-chemical analysis of fermented broth**

##### **High performance liquid chromatography analytical methods (HPLC)**

The filtrate supernatants were analyzed for glucose and erythritol by HPLC under isocratic conditions a refractive index detector (Waters 2414) at 30°C, using an amino column APS-2 Hypersil column. The column was kept at 30°C with a mobile phase constituting of water and acetonitrile (25:75 v/v) at a flow rate of 1 mL min<sup>-1</sup>.

##### **Dry cell weight analytical methods**

Culture broth were centrifuged at 5,000 x g for 15 minutes. The cultured cells were wash twice with sterile distilled water and dried to constant weight in a hot air oven at 105°C (Ghezelbash *et al.*, 2014). The dry cell weight (DCW) was calculated using the following equations.

#### **Statistical analysis**

All data were analysed for ANOVA using SPSS program. The results are means ± S.D. for triplicate experiments and significantly different at 99% (p<0.01)

#### **Results and discussion**

##### **Mutagenesis**

The synergistic effect of UV irradiation and EMS on *Moniliella* sp. BCC25224 in screening for superior erythritol production was investigated. The sequential treatment of *Moniliella* sp. BCC25224 by UV, and immersion in EMS for 15, 30, and 60 min resulted in 3%, 1% and 0% survival of *Moniliella* sp. BCC25224, respectively. Surviving colonies were inoculated in GYE medium and then further analyzed by HPLC. Screening of mutants via culturing in broth for erythritol production and glucose utilization resulted in the selection of three mutants that were *Moniliella* sp. BCC25224-M13, BCC25224-M14 and BCC25224-M15 that produced more erythritol than parent cells (Table 1). A total of 138 survivor mutant colonies were analyzed of which 97.8% produced erythritol at lower amount than did the parent strain (3.8 - 9.3 gL<sup>-1</sup>).

Mutant strains increased in cell mass because of an increase in glucose consumption (Table 1) hence greater metabolic activity increased cell multiplication led to higher erythritol production. Statistically, *Moniliella* sp.

BCC25224-M13 varied significantly ( $p < 0.01$ ) relative to the parent culture. The mutant BCC25224-M14 and BCC25224-M15 produced less erythritol lower than BCC25224-M13 with low glucose consumption (Table 1). Nevertheless, BCC25224-M14 and BCC25224-M15 had similar erythritol yields which were higher than that of BCC25224-M13. The relatively low erythritol yield of BCC25224-M13 was attributed to the high cell mass production during fermentation.

*Candida magnolia* mutant were generated by ultraviolet and EMS chemical mutagenesis (Ghezelbash *et al.*, 2014). The mutant named 12-2 gave a 2.4-fold and 2.2 fold increased in erythritol production ( $20.32 \text{ gL}^{-1}$ ) and yield (10.99%) from  $200 \text{ gL}^{-1}$  glucose compared to the parent strain. The glucose consumption of parent and mutant was 84.87% and 92.41%, respectively. PCR product of the mutant revealed a minor change in the sequence of genes involved in a production pathway which can lead to a significant increase in protein translation.

*Aureobasidium* sp SN-124A successfully mutated with UV irradiation and NTG treatment (Ishizuka *et al.*, 1989). The mutant produced erythritol with 47.6% yield on a medium containing 22.5% glucose compared to 41.8% yield obtained from parent strain. The erythritol

concentration produced reached  $164.8 \text{ gL}^{-1}$  with the mutant while the parent was  $110 \text{ gL}^{-1}$ .

Chemical mutagenesis of *Moniliella* sp. 440 by N-methyl-N'-nitro-N-nitrosoguanidine (NTG) resulted in N61188-12 mutant which produced two times more erythritol ( $237.8 \text{ gL}^{-1}$ ) than parent strain in fermentation medium comprise of  $400 \text{ gL}^{-1}$  glucose and  $10 \text{ gL}^{-1}$  yeast extract (Lin *et al.*, 2010). Although the mutant strain consumed the glucose completely for efficient erythritol production with 55.6% yield, the cell density ( $A_{660}$ ) was lower than parent strain (26.1 and 56.8). The high erythritol production and yield was attributed to the low by-product production e.g. glycerol and ribitol. Glucose concentration produces osmotic stress on biomass and erythritol formation (Jeya *et al.*, 2009).

Although, the improvement in erythritol production of the *Moniliella* sp. BCC25224 in this study was achieved by mutagenesis, the production performance of the mutant was lower than the other erythritol-producing strains. The low production efficiency probably resulted from the small number of cells. Anyway, *Moniliella* sp. BCC25224-M13 was further examined for cell growth and erythritol formation in batch fermentation and compared with the parent strain to confirm the mutagenesis achievement.

**Table 1** Erythritol production of wild type strain and derived mutant at flask scale (Volume of flask) after 5 days of fermentation

| Strain                                  | Dry cell weight ( $\text{gL}^{-1}$ ) | Glucose consumption (%) | Erythritol production ( $\text{gL}^{-1}$ ) | Erythritol yield (%) |
|-----------------------------------------|--------------------------------------|-------------------------|--------------------------------------------|----------------------|
| <i>Moniliella</i> sp. BCC25224 (Parent) | $13.2 \pm 1.0^b$                     | $74.0 \pm 7.8^b$        | $35.1 \pm 3.5^b$                           | $24.7 \pm 3.7^b$     |
| <i>Moniliella</i> sp. BCC25224-M13      | $18.0 \pm 2.0^a$                     | $98.7 \pm 2.3^a$        | $44.2 \pm 0.1^a$                           | $25.6 \pm 0.1^b$     |
| <i>Moniliella</i> sp. BCC25224-M14      | $17.6 \pm 1.3^a$                     | $77.7 \pm 0.3^b$        | $39.1 \pm 0.1^b$                           | $28.7 \pm 1.2^a$     |
| <i>Moniliella</i> sp. BCC25224-M15      | $16.7 \pm 0.6^a$                     | $78.2 \pm 0.9^b$        | $38.8 \pm 0.1^b$                           | $28.4 \pm 0.7^a$     |

Mean values with different letters in columns indicates a significant difference ( $p < 0.01$ )

Results are means  $\pm$  S.D. for triplicate experiments.

### Up-scale production of erythritol in 10 L fermenter

A batch fermentation was carried out for both *Moniliella* sp. BCC25224 and *Moniliella* sp. BCC25224-M13 mutant strain in a 10-L jar fermenter to observe the cell growth, glucose utilization, erythritol production pattern, and especially for erythritol production efficiency. The cell growth, glucose consumption and erythritol production rate should indicate the ideal conditions for the further fed-batch operation. The parent *Moniliella* sp.

BCC25224 and *Moniliella* sp. BCC25224-M13 produced erythritol during cell growth (Figure 1 and 2) and fermentation which indicated that erythritol is a primary metabolite (Sanchez & Demain, 2008). Erythritol is also synthesised during the exponential phase of growth and synthesis is an integral part of the normal growth process. The cells showed continuous growth throughout the cultivation period (216 hours) but during the stationary phase growth could not be clearly determined.

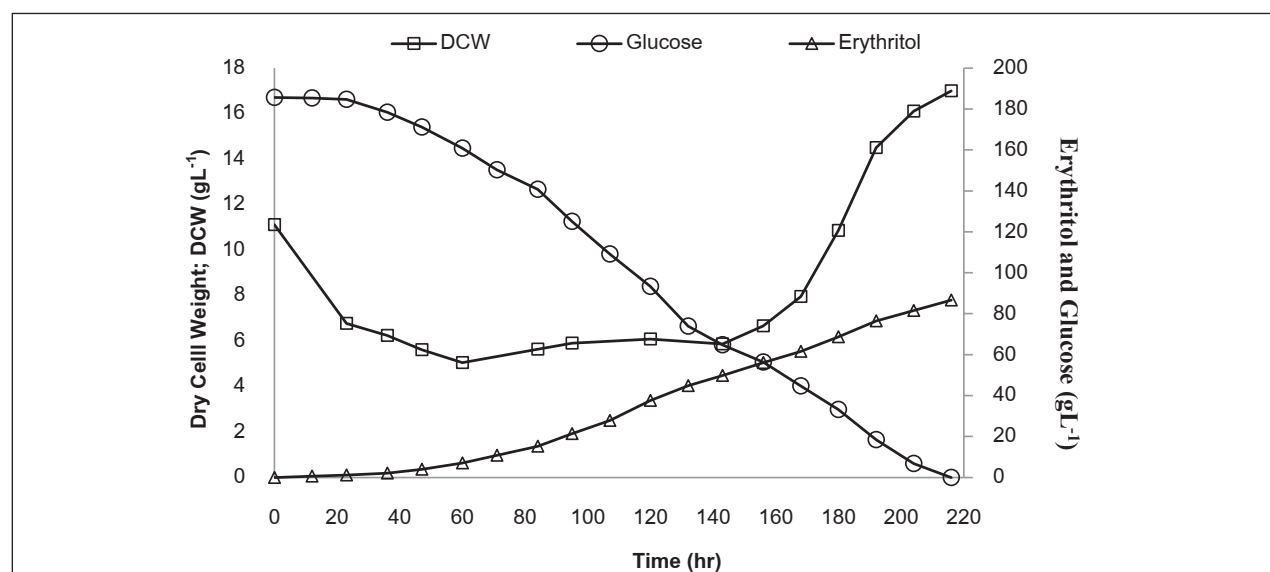
In the first 48 hours of the fermentation, dry cell weight value was interfered with by the soy bean flour. *Moniliella* sp. BCC25224 showed a higher growth rate than the mutant strain after 143 hours ( $0.15 \text{ gL}^{-1}\text{h}^{-1}$  and  $0.07 \text{ gL}^{-1}\text{h}^{-1}$ ). Erythritol formation of the parent and mutant began at 23 hours with different production rates. Glucose was completely consumed by parent and mutant strain after fermentation for 216 and 204 hours respectively, which reflected the lower dry cell weight of the mutant. The pH of fermentation broth of both strains decreased from 5.4 to 4.0 after 48 hours and continued to decrease with the lowest pH value of 3.5 at 95 hours. The rate of growth and of substrate consumed reflected the cell's ability to respond to the environment (Figure 1 and 2). High glucose concentration caused inhibition of cell growth and synthesis of erythritol. Our results agreed with Kobayashi *et al.* (2013) who reported erythritol production in response to oxidative stress and altered redox balance by *Moniliella megachiliensis*.

For the parent strain, the erythritol production, erythritol yield, yield coefficients and volumetric production rate were  $86.6 \text{ gL}^{-1}$ , 46.7%,  $0.47 \text{ gg}^{-1}$  with  $0.40 \text{ gL}^{-1}\text{h}^{-1}$ , respectively. While *Moniliella* sp. BCC25224-M13 produced  $103.5 \text{ gL}^{-1}$  erythritol; 56.9%, erythritol yield;  $0.59 \text{ gg}^{-1}$ , yield coefficients, and  $0.47 \text{ gL}^{-1}\text{h}^{-1}$  volumetric production rate. The effect of UV and EMS immersion was maintained in *Moniliella* sp. BCC25224-M13 as a 1.2-fold increase in erythritol production and yield was observed (Table 2).

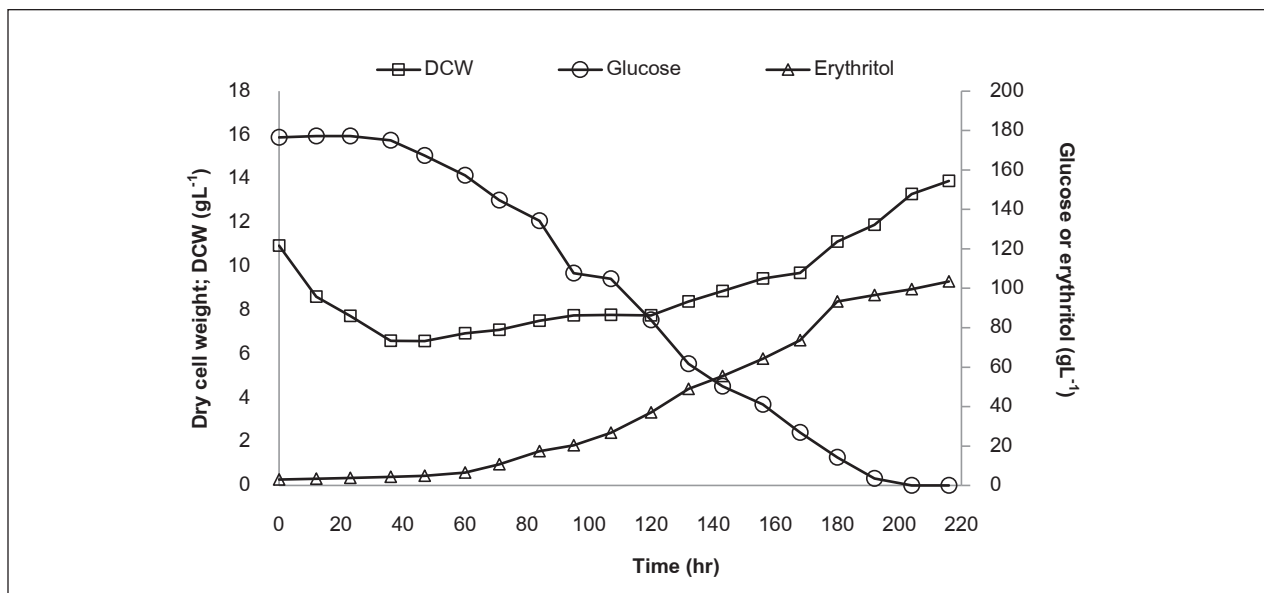
The productivity of *Moniliella* sp. BCC25224-M13 were compared with that of other microorganisms which have been reported previously to produced erythritol (Table 2). *Moniliella* sp. BCC25224-M13 showed similar higher values in terms of erythritol yield and yield coefficients when compared to most other strains cultivated in traditional batch culture. However, erythritol production and productivity is lowest which was similar to the results at flask scale.

Focusing on simple batch culture (Table 2), *Pseudozyma tsukubaensis* gave the highest erythritol production, erythritol yield, yield coefficients and productivity. In addition, Jeya *et al.*, (2009) reported the dry cell weight after fermentation for 36 hours was  $25.2 \text{ gL}^{-1}$  which was higher than with *Moniliella* sp. BCC25224-M13 ( $13.9 \text{ gL}^{-1}$  at 216 hours). Thus, increasing the cell formation during fermentation should result in higher erythritol production.

In the case of fed-batch fermentation, the erythritol productivity was higher than batch fermentation because the batch culture at high glucose level inhibited the maximum volumetric productivity (Rzechonek *et al.*, 2018, Jeya *et al.*, 2009). Maintaining a glucose concentration during fermentation can increase erythritol production and dry cell weight (Jeya *et al.*, 2009). Also, *Moniliella* sp. BCC25224-M13 should maintain the glucose content at  $100 \text{ gL}^{-1}$  during the exponential phase of growth (Figure 2).



**Figure 1** Biomass and erythritol production of *Moniliella* sp. BCC25224 parent strain in 10 L jar fermenter ( $200 \text{ gL}^{-1}$  glucose with  $13 \text{ gL}^{-1}$  soybean flour)



**Figure 2** Biomass and erythritol production of *Moniliella* sp. BCC25224-M13 mutant strain in 10 L jar fermenter (200 gL<sup>-1</sup> glucose with 13 gL<sup>-1</sup> soybean flour)

**Table 2** Erythritol productivity comparison of producing strains in various reactor operation types using glucose as substrate

| Strain                                                              | Operation type          | Erythritol production (gL <sup>-1</sup> ) | Erythritol yield (%) | Yield coefficients (gg <sup>-1</sup> ) | Productivity (gL <sup>-1</sup> h <sup>-1</sup> ) | Reference                                             |
|---------------------------------------------------------------------|-------------------------|-------------------------------------------|----------------------|----------------------------------------|--------------------------------------------------|-------------------------------------------------------|
| <i>Aureobasidium</i> sp. (mutant SN-124A)                           | Batch                   | 170.0                                     | 37.7                 | N.A.*                                  | 1.82                                             | Rzechonek <i>et al.</i> (2018)                        |
| <i>Candida magnoliae</i>                                            | Fed-batch               | 200.0                                     | 43.0                 | N.A.*                                  | 1.2                                              | Rzechonek <i>et al.</i> (2018)                        |
| <i>Candida magnoliae</i>                                            | Two-stage Fed-batch     | 187.0                                     | 41.0                 | N.A.*                                  | 2.8                                              | Rzechonek <i>et al.</i> (2018)                        |
| <i>Candida magnolia</i> JH110 (mutant)                              | Fed-batch               | 200.0                                     | 43.0                 | N.A.*                                  | 1.2                                              | Rzechonek <i>et al.</i> (2018)                        |
| <i>Torula</i> sp.                                                   | Fed-batch               | 192.0                                     | 48.0                 | N.A.*                                  | 2.26                                             | Rzechonek <i>et al.</i> (2018)                        |
| <i>Trichosporon</i> sp.                                             | Batch, Stirred tank     | 138.0                                     | 46.0                 | 0.49                                   | 1.23                                             | Park <i>et al.</i> (1998) ; Jeya <i>et al.</i> (2009) |
| <i>Trichosporon</i> sp.                                             | Fed-batch, Stirred tank | 316.8 <sup>a</sup>                        | 44.0                 | 0.51                                   | 1.33                                             | Park <i>et al.</i> (1998)                             |
| <i>Moniliella megachilliensis</i> sp. 440 mutant (mutant N53199-12) | Batch, Stirred tank     | 152.4                                     | 43.6                 | N.A.*                                  | 0.65                                             | Rzechonek <i>et al.</i> (2018)                        |
| <i>Moniliella</i> 618A-01                                           | Fed-batch, Stirred tank | 100.0                                     | 39.3                 | N.A.*                                  | 0.19 <sup>a</sup>                                | Hirata <i>et al.</i> (1999)                           |
| <i>Moniliella</i> 278-3 (or <i>Moniliella</i> sp. 166-2)            | Batch, Stirred tank     | 111.0                                     | 37.0                 | 0.37 <sup>a</sup>                      | 0.77 <sup>a</sup>                                | Lin <i>et al.</i> (2001)                              |
| <i>Moniliella</i> sp. N61188-12 (mutant)                            | Batch, Stirred tank     | 142.0                                     | 40.5 <sup>a</sup>    | N.A.                                   | 1.18 <sup>a</sup>                                | Lin <i>et al.</i> (2010)                              |
| <i>Moniliella</i> sp. N61188-12 (mutant)                            | Fed-batch, Stirred tank | 189.4                                     | 48.0                 | N.A.*                                  | 0.80                                             | Lin <i>et al.</i> (2010)                              |

**Table 2** Erythritol productivity comparison of producing strains in various reactor operation types using glucose as substrate (cont.)

| Strain                                          | Operation type                | Erythritol production (gL <sup>-1</sup> ) | Erythritol yield (%) | Yield coefficients (gg <sup>-1</sup> ) | Productivity (gL <sup>-1</sup> h <sup>-1</sup> ) | Reference                         |
|-------------------------------------------------|-------------------------------|-------------------------------------------|----------------------|----------------------------------------|--------------------------------------------------|-----------------------------------|
| <i>Moniliella tomentosa</i> var <i>pollinis</i> | Batch, Stirred tank           | 90.0                                      | 36.1                 | 0.35                                   | 0.59 <sup>a</sup>                                | Burschapers <i>et al.</i> (2002a) |
| <i>Moniliella tomentosa</i> var <i>pollinis</i> | Fed-batch, Stirred tank       | 170.0                                     | 38.8                 | N.A.*                                  | 1.62 <sup>a</sup>                                | Burschapers <i>et al.</i> (2002a) |
| <i>Moniliella tomentosa</i> var <i>pollinis</i> | Batch, Airlift tower loop     | 105.0                                     | 62.0                 | 0.40                                   | N.A.*                                            | Burschapers <i>et al.</i> (2002b) |
| <i>Moniliella tomentosa</i> var <i>pollinis</i> | Fed-batch, Airlift tower loop | 175.0                                     | 54.0                 | 0.39                                   | N.A.*                                            | Burschapers <i>et al.</i> (2002b) |
| <i>Moniliella</i> Mutant HAT 101                | Batch, Airlift tower loop     | 150.0                                     | 65.0                 | 0.57                                   | N.A.*                                            | Burschapers <i>et al.</i> (2002b) |
| <i>Moniliella</i> Mutant HAT 101                | Fed-batch, Airlift tower loop | 175.0                                     | 70.0                 | 0.58                                   | N.A.*                                            | Burschapers <i>et al.</i> (2002b) |
| <i>Pseudozyma tsukubaensis</i>                  | Batch, Stirred tank           | 243                                       | 61.0                 | N.A.*                                  | 1.65                                             | Jeya <i>et al.</i> (2009)         |
| <i>Pseudozyma tsukubaensis</i> KN75             | Fed-batch, Stirred tank       | 245                                       | 61.0                 | N.A.*                                  | 2.86                                             | Jeya <i>et al.</i> (2009)         |
| <i>Moniliella</i> sp. BCC25224                  | Batch, Stirred tank           | 86.6                                      | 46.7                 | 0.47                                   | 0.40                                             | this study                        |
| <i>Moniliella</i> sp. BCC25224-M13 (mutant)     | Batch, Stirred tank           | 103.5                                     | 56.9                 | 0.59                                   | 0.47                                             | this study                        |

*Moniliella*, *Trichosporonoides* and *Aureobasidium* sp. were thought to be synonymous

<sup>a</sup> calculation estimation

\* not available

## Conclusions

In this study, *Moniliella* sp. BCC25224 was subjected to UV and EMS mutagenesis. The mutant *Moniliella* sp. BCC25224-M13 produced a higher erythritol concentration and erythritol yield during fermentation with glucose as substrate than in *Moniliella* sp. BCC25224. Sequential random mutagenesis through UV irradiation and EMS treatments were achieved and obtained a potential candidate mutant for erythritol production. Attempts at further erythritol improvement should study process operation to optimize biomass and erythritol production. Erythritol production and productivity should increase influence of osmotic pressure or the glucose concentration regulation.

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